

# ENERGY PRINCIPLE

## Steady Flow Energy Equation

For steady flow, the flow accumulation equal zero and if the velocity distribution is constant, then

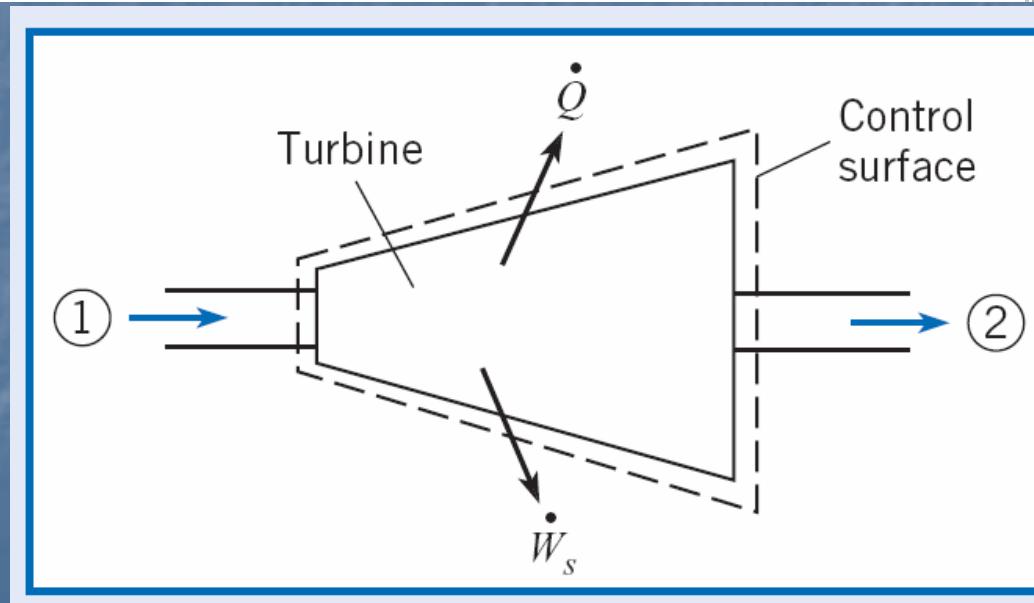
the Eqn.  $\dot{Q} - \dot{W}_s = \frac{d}{dt} \int_{cv} (u + \frac{V^2}{2} + gz) \rho dQ + \int_{cs} (h + \frac{V^2}{2} + gz) \rho V \bullet dA$  becomes

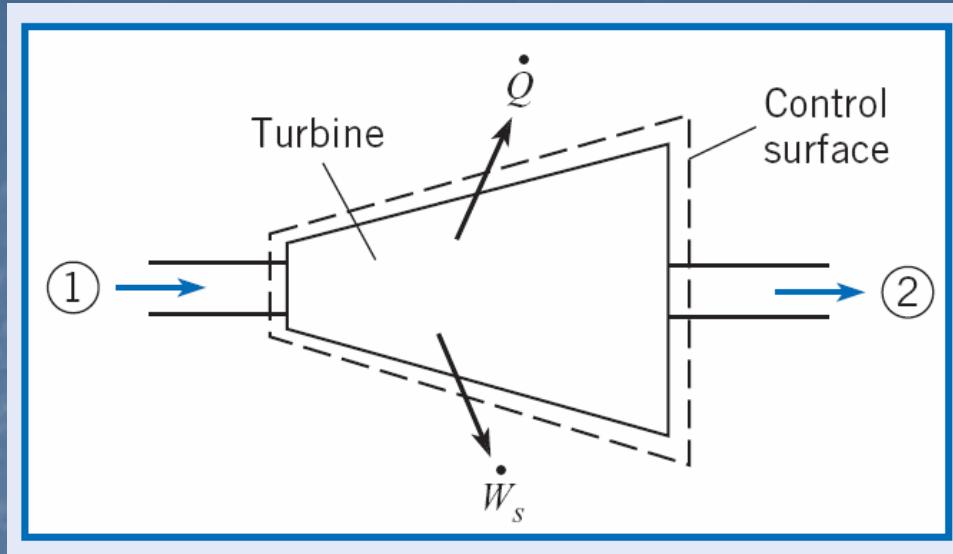
$$\dot{Q} - \dot{W}_s = \sum_{cs} \dot{m}_{out} \left( \frac{V^2}{2} + gz + h \right)_{out} - \sum_{cs} \dot{m}_{in} \left( \frac{V^2}{2} + gz + h \right)_{in}$$

## Example (7.1)

A steam turbine receives superheated steam at 1.4 MPa absolute and 400°C, which corresponds to a specific enthalpy of 3121 kJ/kg. The steam leaves the turbine at 101 kPa absolute and 100°C, for which the specific enthalpy is 2676 kJ/kg. The steam enters the turbine at 15 m/s and exits at 60 m/s. The elevation difference between entry and exit ports is negligible. The heat lost through the turbine wall is 7600 kJ/h. Calculate the power output if the mass flow through the turbine is 0.5 kg/s.

**Solution** First sketch the general layout of the turbine, indicating the inlet and outlet velocities, shaft work, and heat transfer, as shown.





Given:  $h_1 = 3121 \frac{kJ}{kg}$ ,  $h_2 = 2676 \frac{kJ}{kg}$ ,  $V_{in} = 15 \frac{m}{s}$ ,  $V_{out} = \frac{m}{s}$ ,  $\dot{Q} = 7600 \frac{kJ}{kg}$ ,  $z_1 = z_2$ ,

$$\dot{m} = 0.5 \frac{kg}{sec}$$

Find:  $\dot{W}_{Shaft}$  ?

# Applying the steady flow energy equation

$$\dot{Q} - \dot{W}_s = \sum_{cs} \dot{m}_{out} \left( \frac{V^2}{2} + gz + h \right)_{out} - \sum_{cs} \dot{m}_{in} \left( \frac{V^2}{2} + gz + h \right)_{in}$$

$$(gz)_{out} = (gz)_{in} = 0, \quad \dot{m}_{in} = \dot{m}_{out} = \dot{m},$$

$$\dot{W}_s = \dot{Q} + \dot{m} \left( h_1 - h_2 + \frac{V_1^2}{2} - \frac{V_2^2}{2} \right)$$

$$\dot{W}_s = \frac{-7600}{3600} \frac{\text{kJ}}{\text{h}} \frac{\text{h}}{\text{s}} + 0.5 \frac{\text{kg}}{\text{s}} \left[ \frac{15^2 - 60^2}{2 \times 10^3} \frac{\text{kJ}}{\text{kg}} + (3121 - 2676) \frac{\text{kJ}}{\text{kg}} \right]$$

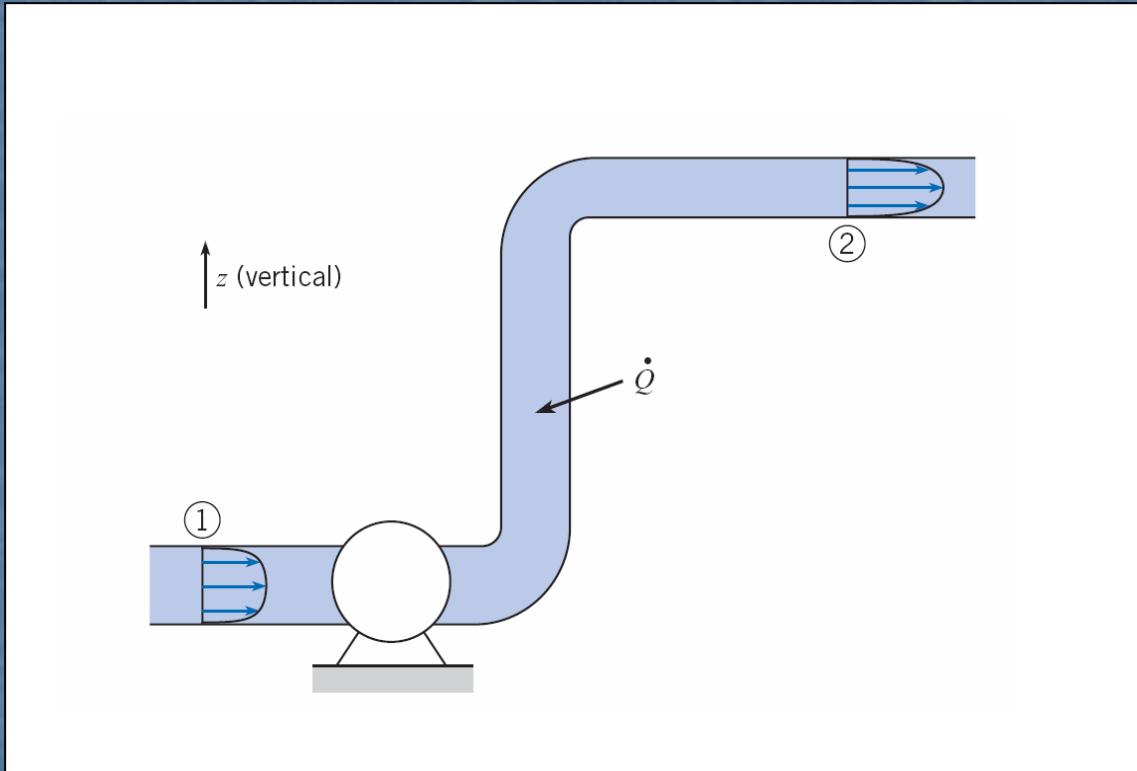
$$= -2.11 + 0.5(-1.69 + 445) = 220 \frac{\text{kJ}}{\text{s}} = 220 \text{ kW}$$

$$\dot{W}_s = 220 \text{ kW}$$

*Note : ( $\dot{Q}$ ) is negative as heat flow out of the system*

# ENERGY PRINCIPLE

## Energy Equation for Steady Flow of an Incompressible Fluid in a pipe



Consider the flow as shown above

## ENERGY PRINCIPLE

The general Energy Eqn. is written as

$$\dot{Q} - \dot{W}_s = \frac{d}{dt} \int_{CV} (u + \frac{V^2}{2} + gz) \rho dQ + \int_{CS} (h + \frac{V^2}{2} + gz) \rho V \bullet dA$$

The energy accumulation term  $\frac{d}{dt} \int_{CV} (u + \frac{V^2}{2} + gz) \rho dQ = 0$  **(Steady Flow)**

$$\dot{Q} - \dot{W}_s = \int_{CS} (h + \frac{V^2}{2} + gz) \rho V \bullet dA \quad \text{where } (h = \frac{p}{\rho} + u)$$

Applying the above equation between section 1 & 2, we have,

$$\dot{Q} - \dot{W}_s = \int_{A2} (h_2 + \frac{V_2^2}{2} + gz_2) \rho V_2 dA_1 - \int_{A1} (h_1 + \frac{V_1^2}{2} + gz_1) \rho V_1 dA_1$$

# ENERGY PRINCIPLE

The term enthalpy =  $h = \left( u + \frac{p}{\rho} \right)$

$$\dot{Q} - \dot{W}_s = \int_{A2} \left( \frac{p_2}{\rho} + u_2 + \frac{V_2^2}{2} + gz_2 \right) \rho V_2 dA_1 - \int_{A1} \left( \frac{p_1}{\rho} + u_1 + \frac{V_1^2}{2} + gz_1 \right) \rho V_1 dA_1$$

$$\dot{Q} - \dot{W}_s + \int_{A1} \left( \frac{p_1}{\rho} + gz_1 + u \right) \rho V_1 dA_1 + \int_{A1} \frac{\rho V_1^3}{2} dA_1 = \int_{A2} \left( \frac{p_2}{\rho} + gz_2 + u_2 \right) \rho V_2 dA_1 + \int_{A2} \frac{\rho V_2^3}{2} dA_2$$

It is common to express the term  $\int \frac{\rho V^3}{2} dA = \alpha \left( \frac{\bar{V}^3}{2} \right) A$

Substituting for  $\int \frac{\rho V^3}{2} dA = \alpha \left( \frac{\bar{V}^3}{2} \right) A$  in Eqn. above and dividing through by  $\dot{m}$

$$\frac{1}{\dot{m}} (\dot{Q} - \dot{W}_s) + \left( \frac{p_1}{\rho} + gz_1 + u_1 + \alpha_1 \frac{\bar{V}_1^2}{2} \right) = \left( \frac{p_2}{\rho} + gz_2 + u_2 + \alpha_2 \frac{\bar{V}_2^2}{2} \right)$$

# ENERGY PRINCIPLE

The coefficients ( $\alpha_1, \alpha_2$ ) are called kinetic energy correction factor and can be evaluated as follows :

$$\alpha \frac{\rho \bar{V}^3 A}{2} = \int_A \frac{\rho V^3 dA}{2}$$

$$\alpha = \frac{1}{A} \int_A \left( \frac{V}{\bar{V}} \right)^3 dA$$

$\alpha = 1$  Velocity is uniform

$\alpha > 1$  Velocity is non-uniform

$\alpha = 2$  Laminar Flow

$\alpha = 1.05$  Turbulent Flow

# END OF LECTURE (2)